The New Era of Waterworks in the 21st Century

Chatan Purification Plant



Advanced Water Treatment Facilities



Water Softening Facility



Water Production by the Advanced System of the New Century

Chatan Purification Plant



The Chatan Purification Plant, located close to the seashore of Chatan Town on Okinawa Island, is the largest purification plant in Okinawa with a daily production capacity of 214,300m³.

The plant is equipped with an advanced water treatment facilities, and designated as the core plant of the West Coast Water Resources Development Project and the Seawater Desalination Project, both of which are promoted by the Okinawa Prefectural Enterprise Bureau.

The facility takes surface waters from the Fukuji Dam, Yamashiro Dam, Kurashiki Dam, Hija River, Nagata River and Tengan River, as well as ground water from Kadena Wells, which are scattered in and around the U.S. Kadena Air Base. In the Chatan Plant, facilities are connected to the central monitoring room by fiber-optic cables, which enable advanced computer control of water operation and management.

Water produced at the plant is supplied to the south of Okinawa City, the southwestern part of the center of the island, and some districts of Naha City.

Address: 1-27 Miyagi, Chatan Town, Nakagamigun, Okinawa

Area:100,254m2

Water Resource:the Fukuji Dam, Yamashiro Dam, Kurashiki Dam, Hija River, Nagata River, Tengan River, and Kadena Wells

Production capacity: 214,300m³ /day (incl. groundwater)

Mainly supplies water to: Chatan Town, Okinawa City, Kitanakagusuku Village, Ginowan City,

Nakagusuku Village, Urasoe City, and Naha City

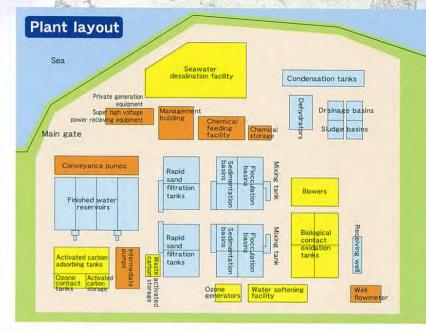
Total construction cost: Conventional water treatment facility: approx. 24.7 billion yen
Advanced water treatment facilities: approx. 22.2 billion yen



Advanced Water Treatment System

The quality of water in the Hija, Nagata. and Tengan Rivers in the middle of the island, from which the plant takes water, suffered deterioration annually, and it became increasingly difficult to treat the water satisfactorily using the conventional treatment process. Therefore, the Enterprise Bureau installed an advanced water treatment plant tentatively to conduct a series of experiments and examinations. The Bureau consequently reached the decision to introduce an advanced treatment system equipped with three processes: biological, ozonation and activated carbon treatments in addition to the conventional treatment process.

First, the biological treatment applies the self-cleansing mechanism of rivers to the water treatment process, in which aerobic bacteria consume organic matter



contained in raw water, achieving a certain purification level. Next, in the ozone treatment, ozone, a gas produced by oxygen reaction in the atmosphere, decomposes organic matter with its deodorizing, bleaching and disinfecting ability due to its strong oxidization power, which is second only to fluorine.

In the final process, granular activated carbon adsorbs odors and organic carbons present, with its high adsorbent quality provided by countless inner micro pores. The activated carbon is a form of carbon produced by baking coal or similar carbon-based matter at a very high temperature.

The combination of the above treatments added to the conventional water treatment system has realized the conversion of highly polluted water into safe, good-tasting water.

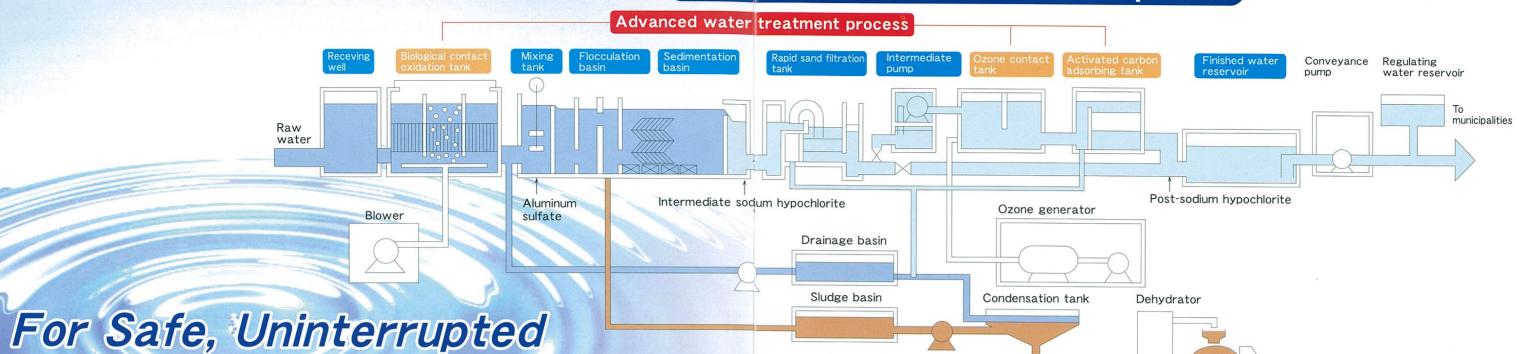
History of Chatan Purification Plant



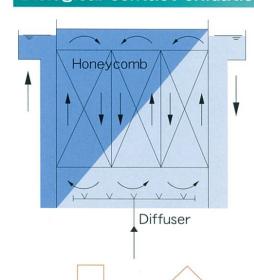
| Year | History | |
|----------------|--|--|
| 1982 | Initiated construction. | |
| 1984 | Set up a water quality examination committee to conduct research into the future projection of water quality on the experimental plant using the advanced weter treatment process. | |
| 1985 | Conducted comparative research into the three biological treatment methods and confirmed the positive effect of the honeycomb aeration method. | |
| 1986 | Completed the 1st stage of construction. | |
| July 1987 | Took in water to the conventional weter treatment facility. | |
| 1986 to1987 | Confirmed the trihalomethane reducing effect of the ozone and activated treatments. | |
| 1987 | Developed the basic plan for an advanced weter treatment facilities. | |
| 1988 | Obtained approval from the former Ministry of Welfare (current Ministry of Health, Labor and Welfare) for the introduction of an advanced weter treatment facilities. | |
| September 1988 | Initiated the construction of a biological treatment facility. | |
| 1990 | Initiated the construction of ozone and activated carbon treatment facilities. | |
| June 1990 | Completed the biological treatment facility and put operation. | |
| 1991 | Partially completed the ozone and activated carbon treatment facilities. | |
| June 1992 | Started partial operation at the advanced weter treatment facility. | |
| 1994 | Completed the advanced weter treatment facilities. | |
| June 1995 | Completed the redevelopment of Kurashiki Dam, and started to intake. Started partial operation at the Seawater Desalination Facility. | |
| 1997 | Completed the Seawater Desalination Facility. | |
| June 2003 | Started operation at the Water Softening Facility. | |

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Flow of advanced water treatment process



Biological contact oxidation tank



Water Supply

Architecture of biological contact membrane

The process applies the self-cleansing mechanism of rivers to the water treatment process, in which aerobic microbes(bacteria) oxidize and decompose matter in water, resulting in the reduction of ammonium nitrogen, algae, musty odor, iron, manganese, anionic surface active agent, etc.

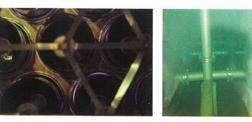
Circulation of water with aeration to activate microbes, to and fro the biological membranes attached to contact material in a honeycomb-like architecture, provides a high water treatment effect equal to the natural self-cleansing mechanism of rivers



Ozone contact tank

Ozone has strong oxidization power, which is capable of disinfecting, deodorizing, bleaching, and oxidizing iron and manganese, as well as decomposing, cyanide, phenols, anionic surface active agent, and humic materials that generate trihalomethanes.

The system sprays ozone-rich air from diffusing pipes, producing highly effective contact with filtered water.



Air cooler & dryer Cooler Ozone generator Dryer To activated carbon adsorbing tank

Ozone production equipment

Production of ozone

For the production of ozone, first dust and particles in the atmosphere are removed. Then, after cooling and drying the air, oxygen is converted into ozone by applying a high voltage (approx. 6,000 to 7,000V) and high frequency (1,000Hz).

Activated carbon adsorbing tank

After the ozone treatment, activated carbon with its high adsorbing capacity adsorbs and removes unsavory odors/tastes/color, and anionic surface active agent, phenols, and organic matter generated during the ozone treatment.

The dissolved oxygen level stays high after the ozone treatment, allowing the microbes developing on the large surface area of granular activated

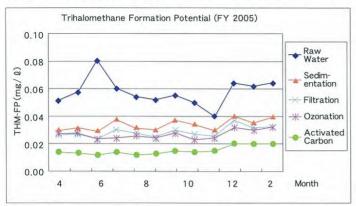




carbon to provide a further decomposing function (biological activated carbon treatment).

Effects of advanced water treatment system

The advanced water treatment facilities at the Chatan Purification Plant comprise three processes: biological treatment, ozonation and granular activated carbon treatment. The biological treatment reduces ammonium nitrogen and levels chlorine demand, which changes significantly from hour to hour. The ozonation decomposes organic matter in the raw water, and the granular activated carbon treatment removes trihalomethane precursors and odorcausing compounds with its high adsorption power and biological activated carbon function. The facilities have been in operation since June 1992, and has shown satisfactory treatment results in regard to trihalomethane and chlorine demand reduction as follows (data as of 2005):



It used to be once difficult to control the amount of trihalomethane at the end of the water supply network below the water quality criteria (0.1 mg/Q) in summer, due to the seasonal rise in water temperature. The introduction of advanced water treatment has realized a substantial reduction in trihalomethane concentration.

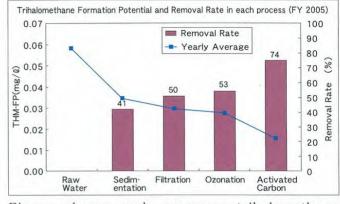
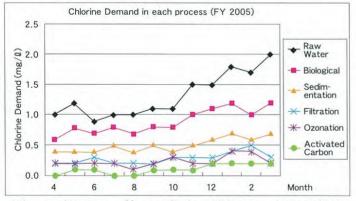
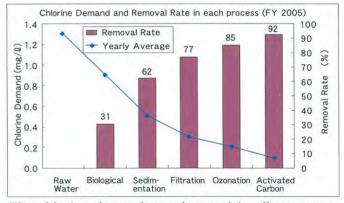


Figure shows each process's trihalomethane formation potential and THM-FP reduction rate compared to that of raw water. The overall removal rate reaches 74 percent.



The reduction effect of the chlorine demand is particularly remarkable in the biological treatment and sedimentation process. The chlorine demand stood at 0.9 to 2.0 mg/2 in the raw water has dropped to 0.1mg/2 in the activated carbon treated water.



The chlorine demands are lowered in all processes and over 90 percent of chlorine demand is removed at the stage of activated carbon treatment. Consequently realizes a substantial reduction in the amount of chlorine dosage.

What is trihalomethane? The purpose of disinfecting drinking water is to remove pathogenic bacteria that cause disease in man. Though disinfection by chlorine has many more advantages than other disinfecting methods, it has a drawback. That is the formation of trihalomethanes (THMs) caused by the reaction of chlorine and organic matter. Their water quality criterion is established along with other tap water standards to ensure safe drinking water. At the Chatan Purification Plant, the advanced water treatment facilities have been introduced to reduce the concentration of THM.

Chlorination is used in water treatment to ensure satisfactory disinfection of potable water supplies. Raw water contains a trace of organic matter. When chlorine is added to the raw water, the chlorine reacts with this matter. In the water treatment at purification plants, sufficient chlorine must be added to completely oxidize such organic matter. A certain amount of chlorine must also remain in the water after the completion of oxidization, so that the effects of the chlorine treatment remain stable. This is called residual chlorine, and the chlorine demand refers to the amount of chlorine required to infuse (in mg/2), until residual chlorine is secured after a certain period of contact with treated water.

Facility Outline

Water Treatment Facilities

| Facility | Specification | | |
|--------------------------------------|--|--|--|
| Receiving well | RC construction: $8.1m \times 19.6m \times 11.3m \times 1 \text{ well}(W \times L \times D)$ | | |
| Biological contact oxidation tank | RC construction: $10.2m \times 10.2m \times 5.0m \times 24$ tanks(alternative aeration honeycomb tube type) | | |
| Mixing tank | RC construction: 4.1m×4.1m×4.1m ×2 tanks | | |
| Flocculation basin | RC construction: 15.2m×27.5m×4.7m ×4 basins(vertical circum flow type) | | |
| Sedimentation basin | RC construction: $26.5m \times 27.5m \times 3.5m \times 4$ basins(horizontal inclined plate type) | | |
| Rapid sand filtration tank | RC construction: 5.0m×10.1m ×32 tanks (50.5m² each) | | |
| Ozone contact tank | RC construction: 8.80m×3.85m×5.0m ×double ×4 tanks | | |
| Activated carbon adsorbing tank | RC construction: 5.0m×10.8m ×16 tanks Layer of granular activated carbon:1.5m thic | | |
| Finished water reservoir | RC construction: 21.6m×52.6m×2.5m ×4 tanks Total capacity:11,000m³ | | |
| Treated water machinery | *Mixing tank stirrer: Flat turbine type *Sedimentation basin sweeper: Underwater towed clarifier | | |
| Chemical feeding facilities | *Aluminum sulfate feeding facilities 390L/hr ×3 injectors 0.6 m³×2 pressure tanks 90m³×3 storage tanks *Sodium hypochlorite feeding facilities 90L/hr ×3 intermediate-injectors 150L/hr ×3 post-injectors 0.6 m³×2 pressure tanks 12m³×2 storage tanks | | |
| Ozone generator | 8.1kg-O ₃ /hr ×4 water-cooling multi-cylinder silent dischrging machines | | |
| Intermediate pump equipment | Horizontal two-way inhalation swirling pumps 33.7m³/min×10m×75kW ×5 pumps | | |
| Conveyance pump equipment | Horizontal two-way inhalation swirling pumps For Yamazato areas: 15.07m³/min×99m×390kW×2, and 15.07m³/min×99m×350kW×3 pumps For Nana areas: 22.13m³/min×100m×570kW×4, and 22.13m³/min×100m×520kW×1 pumps | | |

Power Facilities

| Facility | *Especially high gas insulation locking system (GIS) *Main transformers (infusion auto-cooling type) 4,000KVA×1, and 6,000KVA×1 transformers | |
|--|--|--|
| Super high voltage power receiving and transforming equipment | | |
| rivate generation *Engine: Simple open cycle monopole gas turbine *2,500KVA×2 generators | | |

Wastewater Treatment Facilities

| Facility | Specification | | |
|---|--|--|--|
| Drainage basin RC construction: 15.1m×30.2m×5.8m ×2 basins | | | |
| Sludge basin | RC construction: 11.8m×15.1m×5.8m×2 basins | | |
| Condensation tank | RC construction: 16.9m×16.9m×4.0m×4 basins | | |
| Dehydrator Chemical-free long-term horizontal pressure extractor: 710m² filter cloths×4 Deh 12 m³×4 cake storage hoppers | | | |

Water softening project

Circumstances

The average water hardness of the Chatan Purification Plant is higher than those of other Okinawa Prefectual Enterprise Bureau plants by 100mg/L. This is caused by the Kadena wells' high calcium water hardness resulting from the geological structure of limestone. Water hardness can not be removed by conventional water treatment. And one of the palatable water criterions is the water with hardness between 10 to 100mg/L. So the Water Softening Facility was introduced to the Chatan Purification Plant to treat and soften the Kadena Wells' raw water in FY 2001.

Coping with hard water

OPEB made various investigation to rectify hard water in public water supplies from FY 1985 to FY 1988.

①FY 1985 Investigation of measures to cope with hard waterBasic investigation of feasibility of leveling hardness by mixing soft and hard water (both raw and finished water) and softening water technology

②FY 1986 Experiment of removing hardness from ground water of Kadena wells ... Feasibility investigation of softening by chemicals which gives most satisfactory results in Europe and America

③FY 1987 Second experiment of removing hardness from ground water of Kadena wells ...
Experiment of ion-exchange method and reverse osmosis

④FY 1988 Third experiment of removing hardness from ground water of Kadena wells... Experiment of ①acceleration of chemical softening

2 seawater desalination by ion-exchange

3 water softening by pellet softener

As a result of experiment pellet softening method is adopted for the reason that

(1) high rate of hardness removal

②fewer scaling problems compared with chemical softening method

3 better water quality (speedup of filtration)

@easy to maintain

5 no need to treat wastewater

6 pellets can be used in various ways

⑤ December 2001 Started designing the Water Softening Facility and completed the

design inMarch, 2002

⑥ March 2002 Started constructing the Water Softening Facility⑦ June 2003 Started operation of the Water Softening Facility



Pellet reactor



Injection of seeding grains



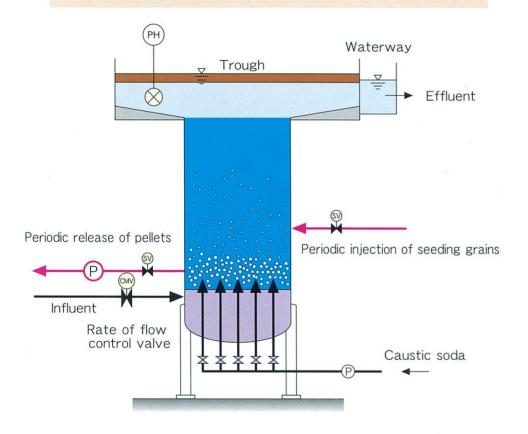
Release of pellets

Basic principles of pellet softeners

Pellet reactors are equipments that efficiently remove water hardness by rapid crystallization of calcium carbonate which takes place in fluidized bed of grains. If the pH is increased to 8 or higher by the addition of alkaline substance, generation of insoluble calcium carbonate occurs. Calcium carbonate tends to adhere and once its scale is formed on the inside of the reactor, it is difficult to remove it. To prevent the formation of scale, seed grains are injected into the water and crystal grows on the seed grains. The grains move freely in the upward flow of the water so that cementing of grains is prevented. During operation the grains in the reactor increase to 1mm to 2mm in diameter. Because large grains have small reactive surface, they should be removed regularly and replaced by smaller-diameter seeding grains.

$$\begin{array}{c} \text{Ca (HCO3)2} + \text{NaOH} \rightarrow \text{CaCO3} \downarrow + \text{NaHCO3} + \text{H2O} \\ \text{Calcium hydrogen carbonate} \end{array} \rightarrow \begin{array}{c} \text{Calcium carbonate} \end{array} \begin{array}{c} \text{Sodium hydrogen carbonate} \end{array} \rightarrow \begin{array}{c} \text{Water} \end{array}$$

Schematic diagram of pellet reactor





Seeding grains



Pellets

Pellet reactor

Softener capacity: 6,800 m³/day/reactor

Number of reactors: 4

| Capacit | ty 6,800m³/d | ay/reactor |
|----------|--------------|------------|
| Velocity | y 100m/hour | |
| Diamet | er φ 1,900mm | ı |
| Height | Reactor | 4.0m |
| | Total heigh | nt 7.0m |
| | | |

| Total hardness | Kadena wells : Raw water 330mg/I Finished water 80mg/I |
|-------------------|---|
| PH | During reaction $8.1 \sim 8.6$ After adjusted $7.1 \sim 7.4$ |

Schematic flow diagram of the water softening facility Softening method Crystallization in a fluidized bed (pellet softening method) Receiving tank Overflow elevation 27,000 m³/day Softening capacity φ 450 HWL +18.600 Effluent PAC mixing tank pH adjustment tank waterway Trough $\nabla + 12.450$ * to Mixing tank Finished water influent pipe Finished φ 400 water Wells' raw water pipe open (M) Rate of flow control valve φ 500 Kadena water wells Trough closed X Rate of filtered water flow control valve Rate of flow control valve φ 200 Filtration tank Finished water Filtration capacity 27,000 m³/day Pellet reactor ϕ 500 Number of tanks 6 Softening capacity 6,800 m³/day/reactor 4.500 m³/day/tank Capacity Seeding grains feeder (\mathbf{M}) Number of reactors 4 Filtration rate 170 m/day Capacity of seeding grains tank 0.3 m³ # from Receiving tank closed to Mixing tank to Secondary Mixing tank Chatan Purification plant to finished water reservoir Water transmission Sedimentation Filtration Finished Advanced basin water treatment water reservoir (M) Carrying out Caustic soda tank Sulfuric acid tank PAC tank Pellet tank Capacity 7m³ Capacity 3m3 Capacity 6m³

E 11 B

Capacity 20m³

10

Outline

| Name | Water Softening Facility |
|-------------------|----------------------------|
| Softener capacity | 27,000 m ³ /day |
| Water resource | Kadena wells |

Water quality

| ltem | Kadena | Kadena | Water |
|-----------------------|----------------------------|-----------------------|-----------------------|
| | wells' raw water | wells' finished water | quality criterion |
| Total hardness (mg/l) | 330 (average 1995~2006) | 80 | 300 no higher than |

Equipment

| Item | Specification | quantity |
|--------------------------|---|----------|
| Pellet reactor | method: crystallizaiton in fluidized bed (pellet softening method) diameter: φ1.9 m height: about 7 m material: SUS304 capacity: 6,800m³/day/reactor | 4 |
| Seeding grains feeder | type: hopper with conical lower part dimensions: ϕ 500mm \times H2,600mm material: SUS304 | 1 |
| Pellet tank | type: lower part discharge hopper dimensions: φ2,900mm×H4,500mm material: SUS304 | 1 |
| Filtration tank | type: gravity rapid filtration method: microfloc process filtration rate: 170m/day | 6 |
| Caustic soda tank | capacity: 7m³ material: FRP | 1 |
| Sulfuric acid tank | capacity: 6m³ material: FRP | 1 |
| PAC tank | capacity: 3m³ material: FRP | 1 |

Structure

| facility | Structure and specification |
|----------------------------|---|
| Pellet reactor bldg. | RC structure, area of total floors: 1,050m ² |
| Receiving tank | RC structure, capacity: 253m3 |
| Filtration wash-water tank | RC structure, capacity: 218m3 |
| Wash-water pumping well | RC structure, capacity: 70m³ |

editor and publisher

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